

## Review on open-problems of spin-up flow of an incompressible fluid

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### Abstract

Open-problems on spin-up flow of an incompressible homogeneous fluid have been reviewed. Characteristics of spin-up are followed by a summary of well-established previous papers along the order: linear spin-up, weakly nonlinear spin-up and non-linear spin-up. Discussions are given to open problems from previous analytic theories as compared with full numerical solutions for Navier-Stokes equation.

**Keywords:** Spin-up flow; Rotating flow; Ekman layer; Stewartson layer; Rossby number

### 1. Introduction

Spin-up refers to the transient adjustment process of a confined fluid when the rotation rate of the container undergoes a change. Specifically, consider an incompressible viscous fluid which fills a closed circular cylindrical container [radius  $R$ , height  $H$ , aspect ratio  $H/R \sim O(1)$ ]. At the initial state, both the fluid and the cylinder are in rigid-body rotation about the longitudinal axis ( $z$ -axis) at rotation rate  $\Omega_i$ . At time  $t=0$ , the rotation rate of the cylinder is increased abruptly to  $\Omega_f (\equiv \Omega_i + \Delta\Omega)$  where the subscript,  $i$ , denotes an initial state and the subscript,  $f$ , a final state. The transient motion of the fluid, in response to this abrupt alteration of the rotation rate of the container, constitutes the spin-up. For the majority of geophysical and technological applications, the flow is characterized by the smallness of the Ekman number  $E$  [ $\equiv v/\Omega_f H^2$ , where  $v$  is the kinematic viscosity of fluid]. The condition  $E \ll 1$  leads to a boundary-layer-type global flow field, which consists of the inviscid interior, the Ekman and Stewartson boundary layers close to the solid walls of the container. For definitiveness, the

cylinder is oriented such that the central longitudinal axis is aligned in the vertical ( $z$ ) axis, and the horizontal direction refers to the radial ( $r$ ) and azimuthal ( $\theta$ ) directions [see Fig. 1].

The pioneering treatise of Greenspan and Howard [1] considered the linear spin-up problem in which the Rossby number  $\varepsilon = \Delta\Omega/\Omega_f$  is very small. By undertaking detailed theoretical analyses, they showed that spin-up is substantially accomplished over the spin-up timescale  $E^{-1/2}\Omega_f^{-1}$ , which is an order-of-magnitude smaller than the diffusive timescale  $E^{-1}\Omega_f^{-1}$ . The main ingredients of the adjustment process are the inviscid-boundary layer interactions, together with the angular momentum conservation in the inviscid interior. The essential flow character has since been verified by numerical simulations and laboratory experiments [see review articles by Benton & Clark (2), Saffman & Baker (3), Duck & Foster (4)].

Efforts were made to extend the linear problem formulation of Greenspan and Howard [1] to nonlinear settings. For  $\varepsilon$  small but finite, Greenspan and Weinbaum [5] carried out series expansions using  $\varepsilon$  to include higher-order terms, which rendered a weakly nonlinear theory. Wedemeyer [6], in a departure from the approach of Greenspan and Weinbaum [5], delineated the character of spin-up flow from the

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initial state of rest, i.e.,  $\Omega_i = 0$ ,  $\varepsilon = 1.0$ . When the container starts rotating from rest, Wedemeyer's solution demonstrated the existence of the radially propagated velocity shear front. The interior inviscid fluid at smaller (larger) radii than the shear front moves toward (away from) the horizontal boundary layers. Venezian [7, 8] generalized the analysis by Wedemeyer to the range  $0 < \varepsilon < 1.0$ . It is important to point out the difficulties associated with the above-stated flow models. The theory of Greenspan & Weinbaum [5] does not recover the nonlinear flow of Wedemeyer in the limit  $\varepsilon \rightarrow 1.0$ . Similarly, the solutions of Wedemeyer [6] and Venezian [8] do not reproduce completely the linear results of Greenspan & Howard [1] as  $\varepsilon \rightarrow 0$ . These are indicative of the challenges ahead in unifying the linear and nonlinear solutions.

In 1970's and 1980's, numerical solutions to the full Navier-Stokes equations were obtained [Watkins & Hussey (9); Kitchen (10); Hyun et al. (11)]. These endeavors verified the global flow field predicted by the previous theoretical studies. Further extensions were made by numerical simulations to explore spin-up with a free surface [Cederlof (12); O'Donnell & Linden (13); Maars (14)], turbulent flows [Cui & Street (15)], in a geostrophic flow [Reznik & Grimshaw (16)], to name a few. Since the 1990's, different aspects of spin-up, somewhat modified from the classical models, were investigated. Examples include spin-up in a non-axisymmetric container [Heijst (17); Suh & Choi (18)]. Also, spin-up flows were delineated when the shapes of the solid walls of the container were deformed. In summary, these are representative of the efforts to tackle more realistic situations.

The present review deals with spin-up flows of an incompressible fluid. Spin-up of a stratified fluid and/or a compressible fluid is a separate topic that has accumulated a considerable body of research [Sakurai (19); Walin (20); Bark et al. (21); Hyun et al. (22); Hyun & Park (23); Park & Hyun (24, 25)].

The longstanding open problems in classical spin-up research may be summarized into the following three categories:

Type-1 open problem: On the viscous effects near the cylindrical sidewall [Benton (26); Konijnenberg & Heijst (27)].

Type-2 open problem: Unifying the prediction of linear and nonlinear flow models [Greenspan & Weinbaum (5); Venezian (7, 8)].

Type-3 open problem: Nonlinear Ekman compatibility condition [Weidman (28); Konijnenberg & Heijst (27)].

In the subsequent review of spin-up flow of an incompressible fluid, the open-problem classified in the above will be remarked in the blanket as [Type-1 open problem], [Type-2 open problem], or [Type-3 open problem] whenever it is revealed.

## 2. General problem formulation

At the initial state, the rotation rate of a fluid and the cylindrical container is  $\Omega_i$ , and the rotation rate of the cylinder is increased instantaneously to  $\Omega_f$  [see Fig. 1]. The Rossby number,  $\varepsilon \equiv \Delta\Omega/\Omega_{ref}$ , where  $\Delta\Omega = \Omega_f - \Omega_i$ , is a measure of nonlinearity. Here, the reference rotation rate,  $\Omega_{ref}$ , is either  $\Omega_f$  or  $\Omega_i$ . For the nonlinear spin-up, it is convenient to set  $\Omega_{ref} = \Omega_f$ , and  $\Omega_i = (1-\varepsilon)\Omega_f$ , as done in [Wedemeyer (6); Venezian (7); Hyun & Park (23)]. In the case of a linear problem, it is customary to select  $\Omega_{ref} = \Omega_i$ ,  $\Omega_f = (1+\varepsilon)\Omega_i$ , as in [Greenspan & Howard (1); Greenspan & Weinbaum (5)]. In the present paper,  $\Omega_{ref} = \Omega_f$ , unless otherwise noted.

The physical quantities of interest are nondimensionalized:

$$(r^*, z^*) = (r/H, z/H), \quad a^* = R/H, \quad t^* = t\Omega_{ref},$$

$$\vec{V}^* = \frac{\vec{V}}{\Omega_{ref}H}, \quad p^* = \frac{p}{\rho(\Omega_{ref}H)^2},$$

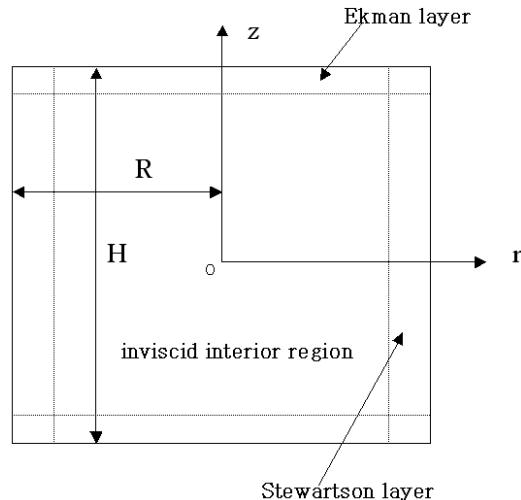


Fig. 1. Coordinates and flow regime in the meridional plane.

The superscript \* represents nondimensional quantities,  $t$  time,  $\vec{V} (\equiv (u, v, w))$  velocity vector in the (radial, azimuthal, axial) coordinate,  $\rho$  fluid density, and  $p$  pressure.

The governing time-dependent axisymmetric Navier-Stokes equations, in nondimensional form, are straightforward, after dropping \*:

$$\frac{\partial u}{\partial t} + u \frac{\partial u}{\partial r} + w \frac{\partial u}{\partial z} - \frac{v^2}{r} = - \frac{\partial p}{\partial r}, \quad (1)$$

$$+ E \left( \frac{\partial^2 u}{\partial r^2} + \frac{\partial}{\partial r} \left( \frac{u}{r} \right) + \frac{\partial^2 u}{\partial z^2} \right),$$

$$\frac{\partial v}{\partial t} + u \frac{\partial v}{\partial r} + w \frac{\partial v}{\partial z} + \frac{uv}{r} = E \left( \frac{\partial^2 v}{\partial r^2} + \frac{\partial}{\partial r} \left( \frac{v}{r} \right) + \frac{\partial^2 v}{\partial z^2} \right), \quad (2)$$

$$\frac{\partial w}{\partial t} + u \frac{\partial w}{\partial r} + w \frac{\partial w}{\partial z} = - \frac{\partial p}{\partial z} + E \left( \frac{\partial^2 w}{\partial r^2} + \frac{1}{r} \frac{\partial w}{\partial r} + \frac{\partial^2 w}{\partial z^2} \right). \quad (3)$$

In the above, the Ekman number  $E \equiv v/\Omega_{ref} H^2$ .

The associated initial and boundary conditions are stated:

$$u = v - (1 - \varepsilon)r = w = 0 \text{ at } t = 0; \quad (4a)$$

$$u = v - r = w = 0 \text{ at } z = \pm 1/2; \quad (4b)$$

$$u = v = \partial w / \partial r = 0 \text{ at } r = 0; \quad (4c)$$

$$u = v - a = w = 0 \text{ at } r = a. \quad (4d)$$

### 3. Flow regime

By inspecting the governing equations, the fact  $E \ll 1$  leads to the assertion that the overall flow field is of boundary-layer-type. It is advantageous to depict the character of the individual flow region [see Fig. 1].

#### 3.1 horizontal boundary layers

The horizontal boundary layer, often termed the Ekman layer, forms near the (horizontal) endwall disks of the container. The fluid in this layer is propelled radially outward due to the increased rotation rate ( $\Omega_i + \Delta\Omega$ ). This, in turn, causes suction in the axial direction of the inviscid interior fluid, which is known as the Ekman pumping. The crux of the argument is that, by way of the Ekman pumping, the rotating disk exerts control of the meridional (secondary)

flow. The thickness of the Ekman layer is scaled  $O(E^{1/2})$ , as can be inferred from the governing equations [Hyun et al. (11); Greenspan (29); Warn-Varnas et al. (30)].

#### 3.2 Vertical boundary layer

The horizontal-propelled fluid flux in the Ekman layer, after reaching the vertical sidewall, is carried vertically along the cylindrical sidewall. Obviously, in order to meet the no-slip condition at the sidewall, a boundary layer is called for. This vertical boundary layer, which is termed the Stewartson layer, is to satisfy the no-slip condition for both the azimuthal and vertical directions. It has been established that the vertical layer consists of a double-layer structure, i.e.,  $O(E^{1/4})$ -layer for the azimuthal flow, and  $O(E^{1/3})$ -layer for the vertical flow. It should be mentioned that, in linear spin-up, the vertical boundary layer is less important in controlling the interior flow. However, in nonlinear spin-up, the influence of the vertical layer is not insignificant in the determination of the interior fluid motion [Barcilon & Stewartson (31); Heijst (32)].

#### 3.3 Inviscid interior region

For  $E \ll 1$ , the thicknesses of the above-stated boundary layers are thin and the bulk of the flow domain is essentially inviscid. In this region, the principal force balance is between the pressure gradient and Coriolis force. Also, the radial and azimuthal velocities are substantially uniform in the axial direction, i.e., the Taylor-Proudman column is maintained [Greenspan [29,33,34]]. Thus, by treating the axial variations of flow properly, there is the possibility that the  $(r, z, t)$  dependent three-dimensional problem can be reformulated as a  $(r, t)$  dependent two-dimensional problem in the inviscid region.

### 4. Linear spin-up

Consideration is given to the transient flow when the rotation rate of the cylinder changes abruptly from  $\Omega_i$  to  $\Omega_f$  [ $\equiv (1 + \varepsilon)\Omega_i$ ]. The problem is linearized under the assumption that the Rossby number  $\varepsilon \ll 1$ . In the original treatise of Greenspan and Howard [1], the governing equations were linearized under  $E \ll 1, \varepsilon \ll 1$ , and an analytical solution was secured by means of the Laplace transform. It should be pointed out that, in Greenspan & Howard [1], the

reference rotation rate of the problem was chosen to be  $\Omega_i$ , not  $\Omega_f$ .

In a short duration  $t \sim O(\Omega_i^{-1})$  after the impulsive start-up of the cylinder, the Ekman boundary layer of thickness  $O(E^{1/2})$  is formed near the endwall disk of the cylinder. A complete mathematical solution is available for the linear Ekman layer, and the scales are  $u \sim O(\varepsilon), v \sim O(\varepsilon), w \sim O(\varepsilon E^{1/2})$ . Also, the axial variations of  $(u, v)$  are well-known spiral structure, as demonstrated in [Greenspan (29)].

In the Ekman layer, the mass flux  $O(\varepsilon E^{1/2})$  of fluid is propelled radially outward; this sucks in the fluid in the inviscid interior. This creates an axial flow,  $w \sim O(\varepsilon E^{1/2})$ , which is termed the Ekman pumping, toward the disk. In the inviscid interior, a concomitant radial flow,  $u \sim O(\varepsilon E^{1/2})$ , is induced. Therefore, in the inviscid interior, in order to satisfy angular momentum conservation, the angular velocity increases by way of vortex stretching, i.e., the spin-up process takes place. The bulk of interior fluid undergoes the spin-up process, and, therefore, the overall adjustment process is substantially accomplished over the spin-up timescale  $O(E^{-1/2})$ , not over the diffusion time scale  $O(E^{-1})$ .

The radial distance ( $d$ ) that a fluid parcel has travelled over the spin-up process is very small, i.e.,  $d \sim O(\varepsilon)$ . This can be inferred from the fact that the distance is the product of the radial velocity scale  $u \sim O(\varepsilon E^{1/2})$  and the spin-up time scale  $O(E^{-1/2})$ .

The time-dependent velocity fields over the spin-up time scale (in the inertial frame) are described approximately [Greenspan & Weinbaum (5)]:

$$v = r + \varepsilon S(2t)r \left(1 - \exp(-E^{1/2}t)\right), \quad (5)$$

$$\Psi/\varepsilon = -rzE^{1/2}S(2t)\exp(-E^{1/2}t). \quad (6)$$

In which  $\Psi$  denotes the meridional stream function ( $u = \partial\Psi/\partial r, w = -\partial\Psi/\partial z$ ), and  $S(t)$  the Fresnel integral,

$$C(t) + iS(t) = \int_0^t (2\pi z)^{-1/2} \exp(iz) dz . \quad (7)$$

The theoretical depiction of linear spin-up has since been validated by a multiple scaling analysis [St-Maurice & Veronis (35)] as well as experiments [Watkins & Hussey (9)] and numerical simulation [Hyun et al. (11)] [see Fig. 2].

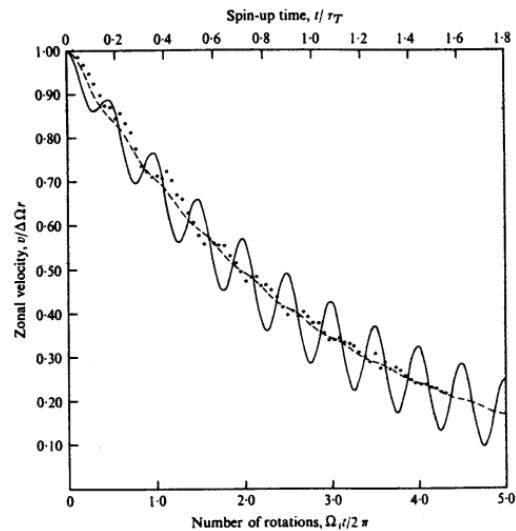


Fig. 2. Comparison of the experiment results ( $E = 3.30 \times 10^{-3}$ ,  $\varepsilon = 0.111$ ) with the analytical results of Greenspan, H.P. & Howard, L.N.(1963) , ●●●●●●●●, experimental data [Warn-Varnas, A., Fowlis, W., Piacs S. & Lee, S.M.(1978)], -----, theory [eq.(3.18) of Greenspan, H. P. & Howard, L. N (1963)], ———, approximate solution [eq. (5)], (printed from Warn-Varnas, A., Fowlis, W., Piacs S. & Lee, S. M. (1978)).

It is to be noted that the spin-up theory of Greenspan & Howard (1963) was developed under the assumption of two infinite disks. This also reinforces the observation that the role of the cylindrical sidewall on the spin-up of interior fluid is insignificant. As remarked previously, the distance that a fluid parcel moves in the linear spin-up is  $d$ , which is much smaller than the thickness of a vertical sidewall boundary layer  $O(E^{1/4})$ , i.e.,  $d \sim O(\varepsilon) \ll O(E^{1/4})$ . It implies that over the duration of spin-up, the fluid originating in the sidewall layer stays in this layer; the influence of the sidewall boundary layer is meager on the interior fluid. For the present closed container, however, a vertical boundary layer exists, and the structure of this layer has been still unveiled so that it makes a challenging research subject [Barcilon & Stewartson (31); Heijst (32)], [Type-1 open problem].

## 5. Weakly non-linear spin-up

For  $\varepsilon$  small, but finite, Greenspan & Weinbaum [5] devised a nonlinear model from the afore-described linear model. They expressed the flow variable by series expansions of the Rossby number  $\varepsilon$ . In the course of analysis, due to the presence of the

secular terms, the strained coordinate method by Poincare and Lighthill was introduced. Due to complications in the analysis, expansions were obtained up to the second-order, i.e.,  $O(\varepsilon^2)$ . The result for the azimuthal velocity is shown:

$$v = r + \varepsilon r (1 - \exp(-2\bar{t})) + O(\varepsilon^2), \quad (8)$$

$$\text{in which } E^{1/2}t = \bar{t} + \varepsilon \left( -\frac{1}{2}\bar{t} + \frac{2}{5}(1 - \exp(-2\bar{t})) \right). \quad (9)$$

This weakly nonlinear model of Greenspan & Weinbaum [5] was shown to be consistent with the experiments in the range  $|\varepsilon| < 0.5$ .

Specifically, two issues are to be stressed:

(1) Because of the nonlinear effect, in comparison to the linear theory, the time to reach the final state becomes shorter (longer) in spin-up (spin-down). Since the theory neglects the higher-order terms, it is not clear if the same conclusion is applicable when  $\varepsilon \sim O(1)$ . However, the later experiments and computations seem to be in support of the qualitative validity of the theory up to  $\varepsilon \sim O(1)$  [34]. However, it will be a challenge to supplement the theory to produce a more versatile analytical model quantitatively [see Fig. 3], [Type-2 open problem].

(2) As stated earlier, the theory of Greenspan and Weinbaum [5] is for two infinite disks with no sidewall. Consequently, this theory is incapable of predicting the presence of the propagating velocity shear front which is a hallmark of nonlinear spin-up in a

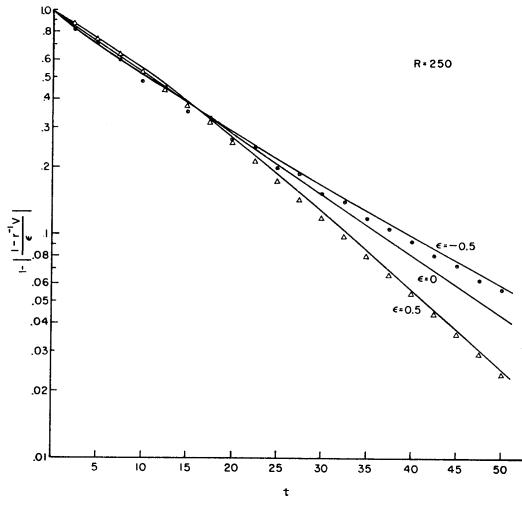


Fig. 3. Comparisons between theory (—) of Greenspan, H. P. & Howard, L. N (1963) and numerical data ( $\Delta$ , ●), (printed from Greenspan, H. P. & Weinbaum, S. (1965)).

confined closed container. This is perhaps a more serious drawback of the theory [Venezian (7, 8)], [Type-1 open problem].

## 6. Non-linear spin-up

### 6.1 Wedemeyer model ( $\varepsilon = 1.0$ )

An elegant theoretical model was put forth by Wedemeyer [6] about spin-up from rest ( $\varepsilon = 1.0$ ). In rapidly rotating flow, the well-known axial uniformity of horizontal velocities in the inviscid interior (Taylor-Proudman column, i.e.,  $\partial u / \partial z = \partial v / \partial z = 0$ ) is exploited. A simplified equation for  $v$  is obtained:

$$\frac{\partial v}{\partial t} + u \left( \frac{\partial v}{\partial r} + \frac{v}{r} \right) = E \left( \frac{\partial^2 v}{\partial r^2} + \frac{\partial}{\partial r} \left( \frac{v}{r} \right) \right) \quad (10)$$

In order to solve the above equation, a relationship linking  $u$  and  $v$  is necessary. To this end, Wedemeyer made use of the numerical result of Rogers & Lance [36]. Furthermore, noting the inter-relations between the inviscid interior flow and the Ekman layer flow, Wedemeyer made the following assumptions:

- (a) the boundary layer flow is quasi-steady;
- (b) the finite geometry of the cylinder does not affect the boundary layer flux;
- (c) the interior fluid is in rigid-body rotation.

Combining the above assumption and the local similarity assumption based on the Rogers & Lance [36]'s data, Wedemeyer arrived at an approximate relationship linking  $u$  and  $v$ :

$$u = E^{1/2}(v - r). \quad (11)$$

Substituting eq. (11) into eq. (10) yields

$$\frac{\partial v}{\partial \tau} + (v - r) \left( \frac{\partial v}{\partial r} + \frac{v}{r} \right) = E^{1/2} \left( \frac{\partial^2 v}{\partial r^2} + \frac{\partial}{\partial r} \left( \frac{v}{r} \right) \right). \quad (12)$$

Under  $E \ll 1$ , dropping the viscous terms in eq. (12) leads to

$$(i) \quad v = 0, w = 2E^{1/2}z, \quad (13a)$$

for the region ahead of the shear front, i.e.,  $r \leq ae^{-\tau}$

$$(ii) \quad v = \frac{1}{1 - \exp(-2\tau)} \left( r - \frac{a^2}{r} \exp(-2\tau) \right),$$

$$w = -\frac{2E^{1/2}z}{\exp(2\tau) - 1}, \quad (13b)$$

for the region behind the shear front, i.e.,  $r \geq ae^{-\tau}$ , where  $\tau = E^{1/2}t$ .

The Wedemeyer solution, Eqs. (13a-b), successfully depicts much of the prominent flow characteristics. The existence of the propagating shear front and the global flow field and other nonlinear behavior are captured well in this model. However, inconsistencies are discernible as well. For instance, the behavior of the Ekman pumping velocity  $w$  in both sides of the front is at variance with assumption (i). Also, the adoption of the numerical data of Rogers & Lance [36] poses a serious difficulty. According to the data of Rogers and Lance [36], the Ekman pumping takes place from the region of small angular velocity to that of large angular velocity. However, the Wedemeyer solution shows that, in the inviscid region behind the front ( $r \geq ae^{-\tau}$ ), the Ekman pumping is directed from the disk-region with a higher rotation rate to the inviscid-region with a lower rotation rate. These, and others, illustrate conflicting assumptions and solutions. The above contradiction casts a question already described in chapter 1 [Type-3 problem]. Despite these shortcomings, the Wedemeyer solution provides overall flow pictures which are shown to be generally compatible with the numerical solutions [Kitchen (10); Hyun et al. (11)]. The inconsistencies of Wedemeyer model have been pointed out [Hyun et al. (11); Benton (26)], but few serious efforts have been made to improve the fundamental foundation of the model.

## 6.2 Extension of the Wedemeyer Model ( $0 < \varepsilon \leq 1.0$ )

Expanding upon the approaches of Wedemeyer [6], Venezian [7, 8] produced an analytical solution for the spin-up from a finite rotation rate ( $\Omega_i \neq 0$ ) to another finite rotation rate ( $\Omega_f \neq 0$ ) for  $0 < \varepsilon \leq 1.0$ :

$$v = \frac{r}{1 + \frac{\varepsilon}{1-\varepsilon} \exp(-2\tau)} \quad \text{at} \\ r \leq a(1 - \varepsilon + \varepsilon \exp(-2\tau))^{1/2}. \quad (14a)$$

$$v = \frac{1}{1 - \exp(-2\tau)} \left( r - \frac{a^2}{r} \exp(-2\tau) \right) \text{ at } \\ r \geq a(1 - \varepsilon + \varepsilon \exp(-2\tau))^{1/2}. \quad (14b)$$

The theoretical solution of Venezian demonstrates the salient nonlinear features for  $\varepsilon \sim O(1)$ , which include the spin-up from rest. However, difficulties

are encountered as this solution attempts to recover the linear spin-up by letting  $\varepsilon \ll 1$ . In addition, it is unclear to come up with a physically convincing explanation about Wedemeyer's assertion that the propagating shear front represents the propagating of characteristic line [Type-1 open problem].

One contribution of Venezian's model lies in the improved treatment of viscous terms in the vicinity of the front. Venezian, by a careful analysis of the thin viscous layer in the neighborhood of the shear front, gave a description of flow surrounding this front:

$$\nu = 4E^{1/4}(2\pi\eta)^{-1/2}(ar\exp(\beta^2)erfc(\beta))^{-1}, \quad (15)$$

in which

$\eta = \exp(2E^{1/2}t) - 1$ ,  $\beta^2 = a^2(r^2 \exp(2E^{1/2}t) - 1)^2 / 8E^{1/2}\eta$ ,  
and  $a$  being nondimensional radius of the container.

The analytical solution of Venezian was shown to be generally compatible with the full Navier-Stokes numerical solutions, as displayed in Fig. 4. Clearly, the viscous solution of Venezian, in comparison to the Wedemeyer inviscid solution, is in better agreement with the numerical results. However, the discrepancies near the shear front are not in substantial.

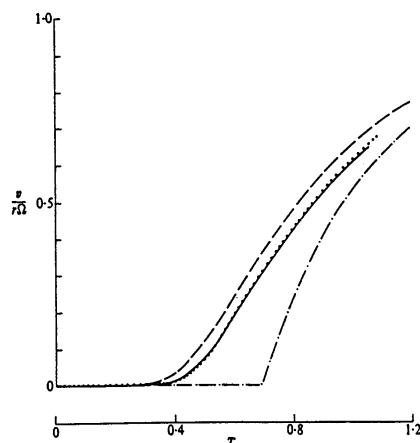


Fig. 4. Time histories of azimuthal velocity ( $E = 9.18 \times 10^{-5}$ ). The vertical location is at mid-depth. The radial location is 0.5

----- Wedemeyer's inviscid solution (Wedemeyer, E.H.(1963));  
 numerical results (Hyun, J.M., Leslie, F., Fowlis, W.M. & Warn-Varnas, A. (1983)); -----, LDV measurements (Warn-Varnas, A., Fowlis, W., Piacts S. & Lee, S. M (1978); -----, Venezian's profile (Venezian, G.(1969)) [eq.(15)], (printed from Hyun, J. M., Leslie, F. Fowlis, W. M & Warn-Varnas, A (1983))

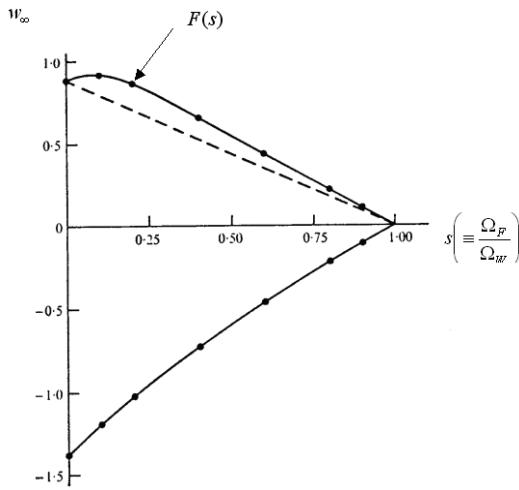


Fig. 5. Nonlinear Ekman pumping velocity.  $w_\infty$  is Ekman pumping velocity at the boundary layer edge,  $\Omega_f$  angular velocity of the far-field fluid and  $\Omega_w$  angular velocity of the disk wall, (printed from Weidman, P.D.(1976)).

### 6.3 The weidman model

Weidman [28] noted that the linear Ekman pumping condition was the source of inconsistencies. From that standpoint, Weidman attempted to use a 7<sup>th</sup>-degree polynomial curve fitting to the numerical data of Rogers & Lance [36] [see Fig. 5].

$$\frac{\partial v}{\partial \tau} + F(v) \frac{\partial(rv)}{\partial r} = 0, \quad (16)$$

in which

$$\begin{aligned} F(s) = & 4.8867s^7 - 21.06589s^6 + 38.23662s^5 \\ & - 38.45380s^4 + 23.88193s^3 - 9.44264s^2 . \\ & + 1.07258s + 0.88446 \end{aligned}$$

Weidman [28] proceeded to make numerical integration and the results contained physically unrealistic flow descriptions near the shear front. In this connection, Benton [26] ascertained an inherent difficulty with the local similarity assumption in utilizing the data of Rogers & Lance [36]. The current trend is to find supplementary ideas to improve or refine the basic model of Wedemeyer. The recent endeavors by Konijnenberg & Heijst [27] also ascertained the need to modify the modeling of Ekman pumping [Type-3 open problem].

## 7. Concluding remarks

The backbone of the modern study of spin-up is the Greenspan & Howard [1] model of linear spin-up ( $\varepsilon \ll 1, E \ll 1$ ). The role of Ekman layer pumping, together with the meridional circulation, is clearly captured in the model. The overall transient process is accomplished over the spin-up time scale  $O(E^{-1/2}\Omega_f^{-1})$ .

The expansion of the model to nonlinear ranges is a challenging issue. The limitation of the weakly nonlinear model is pointed out. The success and shortcomings of the Wedemeyer model ( $\varepsilon = 1.0$ ) are re-visited. The attempts to expand upon or improve this model are discussed.

The classical topic of spin-up is still alive, and some of the future research directions are listed.

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## Nomenclature

$a[\equiv R/H]$	: Aspect ratio of the container,
$E[\equiv \nu/\Omega_f H^2]$	: Ekman number,
$H$	: Height of the container,
$p$	: Pressure,
$r$	: Radial coordinate,
$R$	: Radius of the container
$t$	: Time variable,
$u$	: Radial velocity,
$v$	: Azimuthal velocity,
$w$	: Vertical velocity
$z$	: Vertical coordinate,
$\varepsilon[\equiv \Delta\Omega/\Omega_f]$	: Rossby number,
$\nu$	: Kinematic viscosity of the fluid,
$\Omega$	: Rotation rate of the container,

## superscript

*	: Dimensional variable,
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## subscripts

$f$	: Final state,
$i$	: Initial state,
$ref$	: Reference value.

## References

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